Opportunities and Challenges in Anaerobic Digestion: Maryland and the NE Experience



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AD: Heat Production



- Some (few) farms use recovered heat in a beneficial manner...
- Waste heat usage represents a valuable opportunity for farms

- As much as 75% of the produced heat is wasted
- Excess heat is typically dumped to the ambient using large radiators





Coupling Dairy Manure Anaerobic Digesters with Commercial Greenhouses: An Assessment of Technical and Economic Feasibility





Phase I - Project Goals:

Develop user friendly computer programs to:

- Predict the surplus heat and electricity available from digesters of user specified size, design and operational characteristics. Cornell Anaerobic Digester Simulation Tool
- Predict the required heat and electricity for a greenhouse of user specified size, design and operational characteristics. Cornell Greenhouse Simulation Tool
- Use the output from the AD computer program, and determine the size of greenhouse that could be supported by the specified digester, or the portion of the energy usage of a specified greenhouse that could be digester supported.

Cornell AD/GH Synergy Simulation Tool

Monitoring Surplus Heat Of Digesters







Thanks to:

Dairies

- Synergy Dairy (Covington, NY)
- Stonyvale Farm (Exeter, ME)
- Sunnyside Dairy (Venice, NY)
- Willet Dairy (Locke, NY)
- Commercial Greenhouses
 - Challenge Industries (Ithaca, NY)
 - Durham Foods (Port Perry, ON)

Anaerobic Digester Surplus Heat



Out of Sync Heat Production and Consumption



New York Freestall Barn Dairy Monthly Electricity Use



Source: Adapted from Peterson, Northeast Agriculture Technology Corporation 2014

NY Greenhouse Yearly Electricity Usage



Complementary Electricity Use



Digester Simulation Computer Program

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*			DigDigester – 🗆 × – 🗆 ×	
File	Options Input Simulate Out	put Help	Digester Characteristics	<u>к</u>
	Project Title:	none	Influent incomplete	
	Author:	none	Structure incomplete	
	Input		Equipment DigStructure – 🗆 🗙	
	Project Information	Status Incomplete	Operation Structure Characteristics Help	
	Climate	Incomplete	Digester Shape and Position incomplete	
	Digester	Incomplete	Dimensions	
	Farm	Incomplete		
	Simulate		Insulation incomplete	
			R Values	
			Save Save and Close Close	

Greenhouse Simulation Computer Program

4	Environme	ntalControlSystems - 🛛	
File Options Input Simulate Output	Help	Help	
	ne Heating	Incomplete	
Author: no	Cooling/Venting	Inco	ECSLightControl – 🗆 🗙
InputStatu	S Light/Shade/CO2	Ince Light control method	Help
Project Information Incomp	ete	Supplemental V	Edit Settings
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Structure	lete	Fixture efficiency	
Environmental Control Incomp	lete	PPF from Supplementa	
Crop	lete	Shade control method	Edit Settings
		Shade Transmis	sivity 0.5
		CO2 control method None (natural)	
		Save	Save and Close Cancel/Close

Farm Size	Co Digestion ²	Greenhouse Size	Value of Heat ³	Value of Electricity ⁴	Benefit⁵
(LCE ¹)		(ft²)	(\$/year)	(\$/year)	(\$/year)
	none	580	\$9,975	\$1,650	\$11,625
	10% whey	720	\$11,548	\$2,100	\$13,648
500	25% whey	1,325	\$17,035	\$3,900	\$20,935
	5% FOG	1,125	\$15,107	\$3,300	\$18,407
	10% FOG	1,500	\$18,874	\$4,350	\$23,224
	none	3,250	\$23,170	\$9,600	\$32,770
	10% whey	4,000	\$26,500	\$11,700	\$38,200
1,000	25% whey	6,750	\$31,865	\$19,800	\$51,665
	5% FOG	6,000	\$29,479	\$17,550	\$47,029
	10% FOG	7,500	\$34,316	\$21,900	\$56,216
	none	7,875	\$35,344	\$22,950	\$58,294
	10% whey	9,375	\$39,613	\$27,450	\$67,063
1,500	25% whey	15,500	\$49,345	\$45,300	\$94,645
	5% FOG	13,000	\$43,712	\$37,950	\$81,662
	10% FOG	16,500	\$51,725	\$48,300	\$100,025
	none	14,500	\$46,967	\$42,450	\$89,417
	10% whey	16,500	\$51,725	\$48,300	\$100,025
2,000	25% whey	20,000	\$60,224	\$58,350	\$118,574
	5% FOG	19,000	\$57,424	\$55 <i>,</i> 500	\$112,924
	10% FOG	21,000	\$62 <i>,</i> 879	\$61,350	\$124,229
	none	21,000	\$62,879	\$61,350	\$124,229
	10% whey	28,125	\$69,628	\$82,200	\$151,828
3,000	25% whey	43,750	\$84,545	\$127,800	\$212,345
	5% FOG	33,750	\$73 <i>,</i> 909	\$98,700	\$172,609
	10% FOG	50,000	\$89 <i>,</i> 050	\$146,100	\$235,150

Food Hub Operations Model

Transport seedlings to finish their finish their growth at smaller, distributed operations, located to take advantage of inexpensive heat and power.

Dairy Manure Derived Biogas: Raw Composition

- Methane (CH₄); 55 to 68 percent \rightarrow 60%
- Carbon Dioxide (CO₂); 32 to 45 percent \rightarrow 40%
- Hydrogen Sulfide (H₂S); 1,500 5,000 ppm
- Ammonia (NH₃); 0 300 ppm
- Water Vapor (H₂0); saturated gas: ~4%

Biogas Yields for Sizing Clean-up System

- Cow manure only anaerobic digester systems: 60 to 100 ft³ biogas per lactating cow equivalent on a volatile solids basis (LCE_{vs basis})
- Co-digestion anaerobic digester systems: 2 – 3x cow manure only systems on a LCE_{VS basis} or more
- For existing systems, use gas meter data to size



Potential Biogas Yields



Landfill Biogas: Raw Composition

Dairy Manure Derived Biogas Components plus various other contaminates such as:

Siloxanes
CFCs
S-compounds
Oxygen
Nitrogen

Important Considerations

- End use of biogas/rng and its requirements
- Requirements can drive clean up system method selected
- Clean up systems require energy: electricity and sometimes heat
- CAPEX and OPEX

Important Considerations

- Sometimes no cleanup is cheapest option
- Some methods need redundancy
- Most appropriate solution may include multiple methods arranged in series

Biogas clean-up/upgrading

-Level 1 of 3: Moisture removal

-Level 2 of 3: Hydrogen sulfide removal

-Level 3 of 3: Carbon dioxide removal

Biogas Cleanup – Level 1 of 3 Moisture removal for local use/pipeline transport



Level 1 - Moisture Removal: *Passive Condensation*



Level 1 - Moisture Removal: *Refrigeration*

- Heat exchangers used to cool biogas to desired dew point
- Biogas pressurized to increase further dryness



 Condensate removed from system and disposed of as wastewater

Level 1 - Moisture Removal: Adsorption

- Adsorption agents used to capture moisture
- Silica gel or aluminum oxide used when biogas used for vehicle fuel
- Two vessels are used for continuous
 treatment

Biogas Cleanup – Level 2 of 3

H₂S and moisture (sometimes) reduction for on-site combustion





Level 2 - Hydrogen Sulfide

Sources of Sulfur on Farms <u>Not</u> Importing Food Waste for Co-digestion



Level 2 - Hydrogen Sulfide

Sources of Sulfur on Farms Importing Food Waste for Co-digestion



Level 2 - Hydrogen Sulfide Max. Concentration for Various Biogas End Uses

Designated End Use	Max. [H ₂ S], ppm		
Boiler	1,000		
Engine-Generator	500		
Vehicle Fuel	23		
Pipeline Injection	4		
Fuel Cell	1		

Level 2 - Biogas Hydrogen Sulfide Reduction Options

Digester Influent Additives

- Iron Chloride Dosing
- Ferric Hydroxide Dosing

• Biogas: Physical/Chemical

- Iron Sponge
- Activated Carbon

• Biogas: Microbial

- Biological Fixation

Digester Influent Additive: <u>Iron Chloride (FeCl₂)</u>

- Liquid form Injected directly into digester by an automated dosing unit
- Good for high initial [H₂S] as a first stage of a multistage H₂S removal process
- Comparatively low CAPEX
- Comparatively high OPEX due to chemical cost


Digester Influent Additive: <u>Ferric Hydroxide - Fe (OH)</u>

- Granular, powder, and liquid forms
- Application rate nonlinear, depends on [H₂S] and digester size
- Use started (2013) by NE farm with very good results (3.5 bags/day)
- Google Search reveals price \$600 \$1,500/tonne

Ferric Hydroxide NE Dairy Farm AD





Ferric Hydroxide - Results



Chemical Removal of H₂S: <u>Iron Sponge</u>

- Chemical reaction bonds sulfur to iron oxide
- Reaction occurs at ambient temperatures
- Must be in alkaline conditions, pH > 7.5 w/ 8-10 preferred; caustic soda added as needed
- Temperature < 110F

Chemical Removal of H₂S: *Iron Sponge* (con't)

- Each pound of Fe_2O_3 can remove 0.56 lbs. sulfide
- Iron oxide is impregnate in wood bark: 15
 lbs. Fe₂0₃ per bushel of bark (1 bushel in-place = 1 cu. ft.)

 $3H_2S + Fe_2O_3 + H_2O \rightarrow 4H_2O + Fe_2O_3$



<u>∆p:</u> 2 - 3" wc initially 8 - 10" over time

Iron Sponge – MSU AD System



Two Tank System for Biogas Clean-up



Iron Sponge Scrubbers – Janesville WWTP, Janesville, WI



Chemical Removal of H₂S: Activated Carbon

- Activated carbon impregnated with potassium iodine or sulfuric acid
- Air injected into biogas to promote carbon adsorption of H_2S
- Carbon also regenerated with injected air
- $H_2S \rightarrow$ elemental S

Microbial Removal of Biogas H₂S Biological Fixation

- 2 to 4% air injected into biogas
- Operative microbes grow on surfaces
- Reductions to 60 200 ppm
- Reduces NH₃ as well
- Final [0₂] 0.5 to 1.8% by volume with also Some N due to the injection process





Microbial Removal of H₂S Biological Fixation

 $H_2S + 0.5 O_2 \rightarrow S + H_2O$ (Partial Oxidation)

 $H_2S + 2O_2 + 2OH \rightarrow SO_4 + 2H_2O$ (Total Oxidation)

Thiobacillus sp.

Microbial Removal of Biogas H₂S Biological Fixation

Two Possible Locations:

Digester Biogas Head Space

Separate Vessel







Microbiological Scrubber – Synergy Farm, Covington, NY



Total Annual Cost or Benefit

ΣTotal Annual Costs – (ΣAnnual Cost Savings + ΣAnnual Revenues)

If a <u>positive No</u>., then the system is an economic <u>cost</u> to the farm

If a <u>negative No</u>., then the system is *likely* an economic <u>benefit</u> to the farm

Biogas Cleanup – Level 3 of 3

 H_2S , H_2O , CO_2 , & NH_3 removal for pipeline injection or transportation fuel → "biomethane" or often called "Renewable Natural Gas (RNG)"



Level 3 - Carbon Dioxide (CO₂) Removal – Options

1. Regenerative Water Wash

- 2. Regenerative Amine Wash (Amine)
- 3. Pressure Swing Adsorption (PSA)
- 4. Membrane Separation
- 5. Cryogenic Distillation

Physical Removal of CO₂: Pressure Swing Adsorption (PSA)

 CO₂ is absorbed by means of adsorption materials (molecular sieve)

 This system is used extensively in Germany and Sweeden

Biogas Clean Up - PSA



Biogas Clean Up - PSA





No process water

No wastewater treatment

No chemicals

Removal of H₂O to dew point -90°C



N₂ and O₂ removal

 Hydrocarbon, VOC, and Silicon Compounds removed

• Flexible system, containerized



• Efficient; 97% CH₄ capture

• Off-the-self components

• Very low maintenance

Biogas Clean Up - PSA

(concinentation sewage sign y or game was te)



Biomethane Energy Content

100% CH₄ - LHV = 896 Btu's/scf - HHV = 960 Btu's/scf

Wobbe Index:

- Used to compare the combustion energy output of different composition fuel gases in an appliance
- An indicator of the interchangeability of gaseous fuels

WI = higher heating value/(square root of gas SG)

Average Cost of Biogas Upgrading

Vendor	Biogas Flow (cfm)	Year	Cost (\$/MMBtu)	Technology
Metener	118	2006	6.22	Water Wash
Molecular Gate	142	2008	7.08	PSA
Carbotech	148	2008	10.73	PSA
QuestAir 1 Stage	142	2008	6.73	RPSA
QuestAir 2 Stages	142	2008	7.54	RPSA

Biogas as Liquid Fuel Replacement



Biogas Thermal Energy Value and Diesel Volume Equivalents

Farm	CH ₄	CH₄	Annual Heating	Diesel Eq.
T ann	(%)	(lbs./day)	Value (mmBtu/yr.)	(gal/yr.)
AA Dairy	57	900	7,068,663,000	50,781
New Hope View	58	1,837	14,427,926,590	103,649
Ridge Line	65	3,663	28,769,458,410	206,677
Noblehurst Cell 1 and 2	56	1,069	8,396,000,830	60,316
Patterson	56	3,894	30,583,748,580	219,711
Sunny Knoll	64	1,691	13,281,232,370	95,411











2007 – Dairy Manure Derived Biogas Injection to Natural Gas Pipelines in US

- Few locations attempting this; ID, WI
- Natural gas companies (NGC) very interested
- 17 NGC project investors funded a project in 2007 to develop a US <u>guideline</u> for <u>dairy-based</u> biogas injection

US Guideline for Dairy-Based **Biogas Injection (continued) Biogas testing for:** ✓ Basic composition \checkmark Dissolved metals ✓ Dust \checkmark Microbes – MIC ✓ Others

US Guideline for Dairy-Based **Biogas Injection (continued) Biogas testing for:** ✓ Basic composition \checkmark Dissolved metals ✓ Dust \checkmark Microbes – MIC ✓ Others Guideline Completed 8/2008

2005-2010 Cayuga Renewable Energy, LLC AD/Pipeline/End Use Project





befahrbare Waage
 befahrbare Siloplatten
 Güllevorgrube
 Vorratscontainer für Fermenter
 Fermenter
 Fermenter
 Nachgärbehälter
 Blockheizkraftwerk-Container
 Holzhackschnitzelhalle

6

 Container mit Holzhackschnitzelofen und Wärmeverteilung

5

- 10 Ölkesselcontainer
- 11 Wärmepufferspeicher für das Nahwärmenetz
- 12 Transformatorhaus für Stromeinspeisung
- 13 Feuerlöschteich
- 14 Überlaufbecken
- 15 Warte
- 16 Nahwärmenetz in der Straße nach Jühnde

Luftbild der Bioenergieanlage in Jühnde

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Why are you here? Perhaps...

- For networking opportunities
- ✓ To share knowledge
- Looking for new opportunities
- ✓ Representing products/services for sale
- ✓ To learn
- ✓ Seeking a business opportunity

